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Instabilities of a liquid layer locally heated on its free surface

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We report experimental results concerning patterns in a model experiment built to study buoyant-thermocapillary-driven flows. The fluid is situated in a cooled cylindrical container and locally heated on its free surface. The resulting temperature gradient induces a basic flow which draws the surface fluid from the hot center toward the cold boundary. When the gradient is increased and depending on the height of liquid, the basic flow destabilizes into different stationary patterns. Above a second threshold, the patterns become time-dependent. These different instabilities are characterized and compared to recent theoretical results. © 1997 American Institute of Physics. [S1070-6631(97)02105-3]

In the last decade, the behavior of buoyancy and thermocapillary-driven flows has received much attention both on fundamental and applied aspects. A linear stability analysis was carried out on thermocapillary flows, first without gravity,^{1,2} then in the presence of buoyancy.³⁻⁶ These works show that the basic flow becomes unstable toward longitudinal rolls or hydrothermal waves. Experiments have been performed on fluid layers with free surface subjected to a horizontal temperature gradient both in rectangular^{7,8} and cylindrical⁹⁻¹¹ containers. Some of the theoretical predictions have been recovered, such as the existence of hydrothermal waves, but many points still need to be clarified. This fundamental research is supported by the need for understanding the thermal and hydrodynamical properties of such flows in many applications such as floating zone crystal growth,¹² electron-beam vaporization¹³ or laser welding. However, the real configurations are different from the theoretical ones. In particular, in the last two applications, the liquid is not driven by a horizontal thermal gradient on all its height but only on its surface. In this paper, we report new experimental results concerning the destabilization of a flow locally heated on its free surface. First, we describe the experimental set-up. Then we characterize the different instabilities which depend on the height of liquid and on the temperature difference. Finally, we discuss the experimental results and compare them with available theoretical studies.

The apparatus consists of a cylindrical container made of copper (diameter $2R_0 = 10$ cm and height $h_0 = 4$ cm; see Fig. 1). The bottom is made of sapphire to allow visualization. The container is thermally regulated by circulating water and a Plexiglass plate is situated a few millimeters above the free surface to reduce evaporation. It is filled with silicone oil (viscosity $\nu = 0.0065$ Stokes) of Prandtl number $P = 10$ to a height h that is measured with a precision of 0.02 mm. A meniscus is present at both boundaries. With the lid, h remains constant to 1% over an experimental run. The liquid is locally heated on its surface by a cylindrical heater (diameter $2r_0 = 3$ cm). The two parameters which control the experiment are h and the temperature difference ΔT between the heater and the boundaries. The flow is characterized by temperature (thermocouples) and velocity (LDV) measurements

and by shadowgraphy. The patterns are visualized by shadowgraphic imaging: A parallel vertical light beam crosses the container from bottom to top and forms a picture on a screen, due to surface deformations at the oil-air interface and to horizontal temperature gradients in the fluid. The spatio-temporal evolution of the structures is recorded using a video camera and the images are digitized along a circle to follow the azimuthal evolution of the patterns.⁸

The structure of the flow and the different observed patterns are shown on the stability diagram of Fig. 2. Each experiment is performed with h fixed and ΔT variable. The thermocapillary and the buoyancy effect can be characterized by the Marangoni number $Ma = -(\partial\sigma/\partial T)\Delta Th/\rho_0\kappa\nu$ and the Rayleigh number $Ra = g\alpha\Delta Th^3/\kappa\nu$, where g is the gravitational acceleration, α the thermal expansion coefficient, κ the thermal diffusivity, ρ_0 the density of the fluid, ν the kinematic viscosity and σ the surface tension.

Whatever the height of liquid h , a basic flow is present when ΔT is increased above zero (domain BF in Fig. 2). This flow is due to the thermocapillary effect and draws the surface fluid from the hot center towards the cold boundary. For large values of h ($h = 15$ mm), Fig. 3 gives the radial velocity V_r as a function of the depth z . The velocity is zero for $z < -8$ mm and temperature measurements show horizontal isotherms in this zone. The thermocapillary effect creates a shear flow for $-3 < z < 0$ mm and a return flow is present for $-8 < h < -3$ mm. The basic flow thus appears as a torus and is in fact two dimensional (2D).

When ΔT is increased above a first threshold, whose value varies with h , the basic flow becomes unstable and stationary patterns are observed. Depending on h , three types of patterns are displayed. For small h ($h < 2.8$ mm), a multi-roll state made of co-rotating rolls is encircled by the basic flow and the resulting flow remains 2D [cf. domain CR in Fig. 2 and Fig. 4(a)]. These rolls are present near the heater. The number of rolls decreases with increasing h (3 rolls for $h = 2$ mm) and their wavelength is $\lambda \approx 2.5h$. For intermediate h ($3.2 < h < 5$ mm), the increase of ΔT leads to a pattern with stationary "petals" [cf. domain SP in Fig. 2 and Fig. 4(b)]. The radial extension of the petals is always less than $2R_0/3$ and their number decreases with h from 14 for

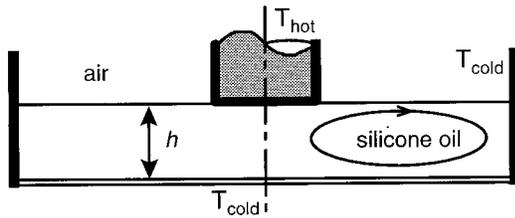


FIG. 1. Schematic drawing of the experimental apparatus.

$h = 3.2$ mm to 11 for $h = 5$ mm. The azimuthal invariance is broken and the resulting flow is 3D. The transition from co-rotating rolls to petals displays intermediate structures near $h = 3$ mm, where $Ra \sim Ma$. For large h ($h > 5.3$ mm), stationary radial structures appear [cf. domain SR in Fig. 2 and Fig. 4(c)]. For $h = 10$ mm, the threshold corresponds to $Ma = 1.7 \times 10^5$ and $Ra = 2.1 \times 10^6$. Contrary to petals, the rays have a small azimuthal extension, they reach the cold vertical boundary and they do not extend over the whole depth. Their number decreases from 11 for $h = 5.3$ mm to 9 for $h = 30$ mm. The rays correspond to counter-rotating rolls (with radial axis) which are superimposed on the basic flow, giving rise to a fully 3D state. The amplitude of the variation of V_r increases with ΔT above the threshold.¹⁴

The patterns become time-dependent above a second threshold. For small h , azimuthal waves are observed very near the heater (cf. domain HW in Fig. 2). They consist of a source emitting a clockwise and an anti-clockwise rotating wave towards a sink. For $h = 2$ mm, 17 rotating structures are evidenced at threshold and the associated frequency is $2\nu/h^2$. The co-rotating rolls are slightly distorted by these waves. For higher ΔT , radial pulsations are observed. For intermediate h , the stationary petals propagate azimuthally [cf. domain RP in Fig. 2 and Fig. 5(a)]. For $h = 4.3$ mm, the azimuthal velocity of the pattern is $8.4\nu/h$ at $r = 19.3$ mm. For large h , the stationary rays oscillate azimuthally [cf. domain OR in Fig. 2 and Fig. 5(b)]. For $h = 10$ mm, the threshold corresponds to $Ma = 4.0 \times 10^5$ and $Ra = 5.0 \times 10^6$. The frequency of oscillation f_0 increases with ΔT . For $h = 6.3$ mm and $\Delta T = 11$ K (resp. $h = 15.2$ mm and $\Delta T = 7.5$ K) $f_0 = 2.9\nu/h^2$ (resp. $f_0 = 14.6\nu/h^2$). When the temperature difference is further increased, the dynamic becomes more complex and the system exhibits spatio-temporal chaos.

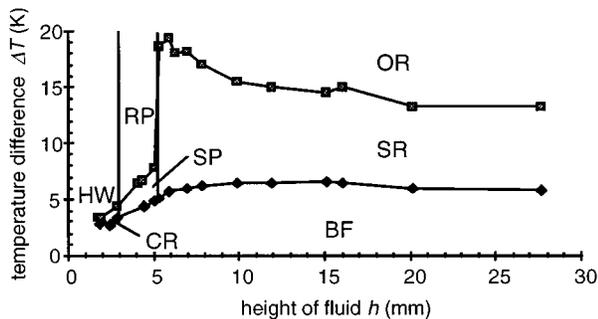


FIG. 2. Stability diagram: temperature difference ΔT_c vs height of liquid h . See text for details.

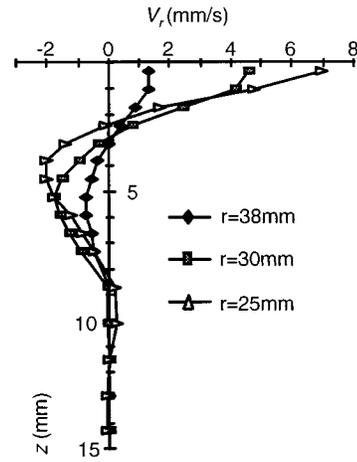


FIG. 3. Radial velocity profile at three different radii r ; $h = 14.6$ mm and $\Delta T = 2.9$ K.

These results raise several interesting hydrodynamic issues. When h is large, the basic toric flow develops only in the upper part of the liquid layer and for $h < -8$ mm, the fluid is at rest. This is due to a stable vertical stratification of the thermal field in the bottom of the cell. Experimental¹⁵ (resp. numerical¹¹) results have displayed this stratification when $A = 1$ (resp. $A \geq 0.75$). In our configuration, this fact becomes important when A exceeds 0.3. Numerical simulations^{3,7} and experiments^{7,9} for small h and various P have shown the multi-roll state, but the understanding of the origin of this state is still lacking. We interpret these rolls as being due to the dynamic interaction between the shear flow and the bottom. For typical critical values of ΔT , the shear layer extends over the first 3 mm which exceeds the depth of fluid: The return flow of the basic torus cannot settle, hence the multi-rolls flow.

The rays correspond to rising hot fluid. This pattern appears when the height of liquid is quasi-infinite. However, the effect of the condition at the bottom is still present for $-10 < h < -5$ mm, as shown by the reduction of their number (from 11 to 9 when h increases) and by the decrease of the second critical curve of Fig. 2. For $h \geq 10$ mm [i.e., for aspect ratios $A = h/(R_0 - r_0) \geq 0.3$], ΔT_c is independent of h . This result is in agreement with the results of Kamotani *et al.*¹¹ for $A > 0.75$ and extends them. The rays could be related to an inversion of the vertical temperature profile near

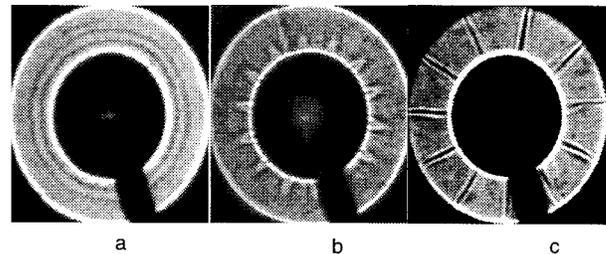


FIG. 4. Shadowgraphic images of the patterns in a horizontal plane. (a) for $h = 1.8$ mm and $\Delta T = 3.2$ K; (b) for $h = 4.3$ mm and $\Delta T = 6$ K, (c) for $h = 15.0$ mm and $\Delta T = 10$ K.

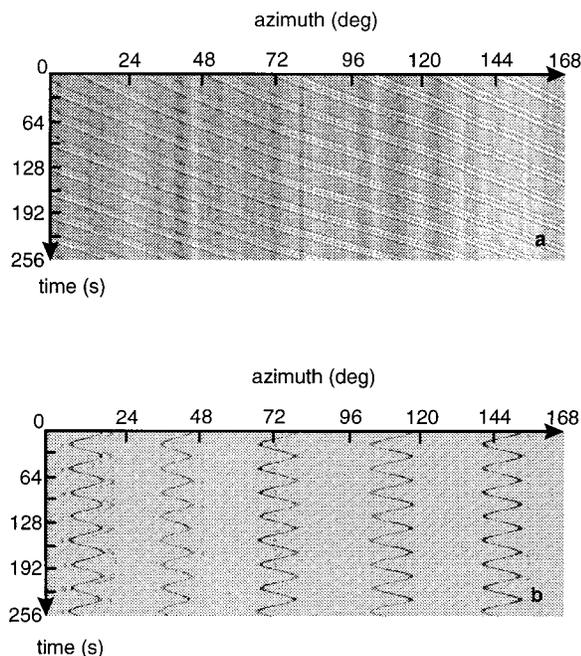


FIG. 5. Spatio-temporal evolution of (a) rotating petals ($h=4.3$ mm); (b) oscillating rays ($h=15.0$ mm).

the free surface and the cold wall, leading to a Bénard–Marangoni instability type, with a critical Marangoni number $Ma_c \approx 600$. This number is far greater than in the pure case where $Ma_c \approx 80$, because of the presence of the basic flow. Stationary rolls of Marangoni type have been found in some models, but associated with a linear flow¹ or never critical.⁶ In the light of the interaction between the basic flow and the condition at the bottom, we propose the petals to be the pattern which develops when the bottom is situated in the extension of the upper part of the return flow (i.e., $-5 < h < -3$ mm).

For small heights, the dynamic states can be quantitatively compared to hydrothermal waves as defined in Refs. 1 and 6 and observed in Refs. 8 and 9. In fact, our results are closer to those of a recent study⁶ which takes into account the influence of thermal boundary conditions and geometry in the selection of the instability. The radial pulsations exhibited for higher ΔT are similar to those observed in Ref. 10 and could be due to a different instability.¹⁴ For larger heights, the observed time-dependent regimes do not correspond to available theoretical results and further work is needed. Let us note that the study of the hysteresis phenomenon of the transition to dynamic states for petals or rays

reveals the subcritical nature of the bifurcation, whereas the primary instability is supercritical whenever h . The amplitude of the oscillations of the rays as well as the velocity of the petals increases with the distance from threshold.

In a liquid layer locally heated on its free surface, the basic 2D flow destabilizes into different patterns depending on the aspect ratio. These patterns have been experimentally characterized, as well as their transition to dynamical regimes. The structures observed at small height are similar to those observed in pure horizontal thermal gradient configurations both in experiments and theories. On the other hand, the patterns observed for larger heights appear to be new and fully 3D. Work is under progress in this direction.

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